1. An integrated Fischer-Tropsch process comprising the steps of:

(a) producing a synthetic crude by Fischer-Tropsch reaction of synthesis gas;

(b) fractionating the synthetic crude at least into a light Fischer Tropsch liquid, and a heavy Fischer Tropsch liquid wherein the light Fischer-Tropsch liquid comprises alcohols;

(c) contacting at least a part of the light Fischer Tropsch liquid with a dehydration catalyst to dehydrate alcohols in the light Fischer Tropsch liquid to corresponding alpha- and internal-olefins to form a dehydrated product;

(d) oligomerizing in an oligomerization reactor all or part of the dehydrated product produced in step (c) to form a product comprising a heavy branched olefin stream;

(e) hydroprocessing the heavy Fischer-Tropsch liquid to form a heavy crude baseoil; and

(f) introducing the heavy branched olefin stream and crude baseoil into a hydrofinisher to produce a synthetic lubricant crude basestock.

2. The process of claim 1 wherein the hydroprocessing step (e) comprises the steps of:

(e1) hydrocracking the HFTL;

(e2) hydrodewaxing all or part of the hydrocracked HFTL; and

(e3) fractionating the product of (e2) to recover a heavy crude baseoil.

3. The process of claim 1 wherein the hydroprocessing step (e) comprises the steps of:

(e4) hydrotreating the HFTL to form a hydrotreated HFTL;

(e5) hydrocracking the hydrotreated HFTL;

(e6) hydrodewaxing all or part of the product of (e5); and

(e7) fractionating the product of (e6) to recover a heavy crude baseoil.

4. The process of claim 1 wherein the hydroprocessing step (e) comprises the steps of:

(e8) hydrocracking the HFTL to form a hydrocracked HFTL;

(e9) fractionating the hydrocracked HFTL to recover a lighter and a heavier fraction;

(e10) recycling a portion of the heavier fraction from step (e9) into the hydrocracker of step (e8); and

(e11) hydrodewaxing the hydrocracked heavier fraction from step (e10).

5. The process of claim 1 wherein the dehydrated light Fischer-Tropsch liquid produced in step (c) is fractionated to recover a C_9-C_{18} fraction and wherein the C_9-C_{18} fraction is oligomerized in step (d).

6. The process of claim 1 wherein the oligomerization of step (d) is catalyzed by a BF_3/co-catalyst system.

7. The process of claim 6 wherein the co-catalyst is an oxygen containing compound.

8. The process of claim 7 wherein the co-catalyst is selected from the group of mono-alcohols, glycol ethers, and polyglycol ethers.

9. The process of claim 1 wherein the oligomerization of step (d) occurs at temperatures from about 50° to about 300°F.

10. The process of claim 6 wherein the BF_3 is present in an amount from about 10 to about 150 parts per one-thousand parts of reactant by weight and the co-catalyst is present in an amount from about 10 to about 200 parts per one-thousand parts of reactant by weight.

11. The process of claim 1 wherein the oligomerization of step (d) is catalyzed by a catalyst system selected from the group of $AlCl_3$/co-catalyst, H_3PO_4, and solid acidic resin catalysts.

12. The process of claim 1 wherein the dehydrated product of step (c) is fractionated to recover a C_9-C_{13} fraction and wherein the C_9-C_{13} fraction is the dehydrated light Fischer-Tropsch liquid used in step (d).

13. The process of claim 1 wherein the dehydrated light Fischer-Tropsch liquid produced in step (c) is fractionated to recover a C_{14}-C_{18} fraction and wherein the C_{14}-C_{18} fraction is oligomerized in step (d).

14. The process of claim 1 further comprising the step of isomerizing at least a part of the dehydrated product of step (c) prior to oligomerization in step (d).

15. The process of claim 1 wherein the synthesis gas is produced by autothermal reaction in the presence of nitrogen.

16. The process of claim 1 wherein the dehydration catalyst is selected from the group of treated activated alumina and treated activated silica-alumina.

17. The process of claim 1 further comprising the steps of:

(g) fractionating the product of step (d) to isolate a nonoligomerized olefin/paraffin stream; and

(h) dehydrogenating the nonoligomerized olefin/paraffin stream by contacting it with a dehydrogenation catalyst.

18. The process of claim 17 wherein the dehydrogenation catalyst comprises a Group VIII metal supported on a high-surface inorganic support.

19. The process of claim 17 further comprising the step of:

(i) passing the product of step (h) into the oligomerization reactor.

20. The process of claim 1 further comprising the step of fractionating the synthetic lubricant crude basestock to recover a synthetic lubricant basestock product containing essentially no unsaturated hydrocarbons and essentially no hydrocarbons having a carbon number of less than 15.

21. An integrated Fischer-Tropsch process comprising the steps of:

(a) producing a synthetic crude by Fischer-Tropsch reaction of synthesis gas;

(b) fractionating the synthetic crude at least into a light Fischer Tropsch liquid, and a heavy Fischer Tropsch liquid wherein the light Fischer-Tropsch liquid comprises alcohols;

(c) subjecting at least some of the light Fischer-Tropsch liquid to means for dehydrogenating hydrocarbons to produce a dehydrogenated light Fischer-Tropsch liquid;

(d) oligomerizing in an oligomerization reactor at least a portion of the dehydrogenated light Fischer-Tropsch liquid to form a product comprising a heavy branched olefin stream;

(e) hydroprocessing the heavy Fischer-Tropsch liquid to form a heavy crude baseoil; and

(f) introducing the heavy branched olefin stream and heavy crude baseoil into a hydrofinisher to produce a synthetic lubricant crude basestock.

22. The process of claim 21 wherein the hydroprocessing step (e) comprises the steps of:

(e1) hydrocracking the HFTL;

(e2) hydrodewaxing all or part of the hydrocracked HFTL; and

(e3) fractionating the product of (e2) to recover a heavy crude baseoil.

23. The process of claim 21 wherein the hydroprocessing step (e) comprises the steps of:

(e4) hydrotreating the HFTL;

(e5) hydrocracking the hydrotreated HFTL;

(e6) hydrodewaxing all or part of the product of (e5); and

(e7) fractionating the product of (e6) to recover a heavy crude baseoil.

24. The process of claim 21 wherein the hydroprocessing step (e) comprises the steps of:

(e8) hydrocracking the HFTL;

(e9) fractionating the hydrocracked HFTL to recover a heavy crude baseoil and a heavier fraction;

(e10) recycling a portion of the heavier fraction from step (e9) into the hydrocracker of step (e8); and

(e11) hydrodewaxing the hydrocracked heavier fraction from step (e10).

25. The process of claim 21 wherein the dehydrated light Fischer-Tropsch liquid produced in step (c) is fractionated to recover a C_9-C_{18} fraction and wherein the C_9-C_{18} fraction is oligomerized in step (d).

26. The process of claim 21 wherein the oligomerization of step (d) is catalyzed by a BF_3/co-catalyst system.

27. The process of claim 26 wherein the co-catalyst is an oxygen containing compound.

28. The process of claim 27 wherein the co-catalyst is selected from the group of mono-alcohols, glycol ethers, and polyglycol ethers.

29. The process of claim 21 wherein the oligomerization of step (d) occurs at temperatures from about 50° to about 300°F.

30. The process of claim 26 wherein the BF_3 is present in an amount from about 10 to about 150 parts per one-thousand parts of reactant by weight and the co-catalyst is present in an amount from about 10 to about 200 parts per one-thousand parts of reactant by weight.

31. The process of claim 21 wherein the oligomerization of step (d) is catalyzed by a catalyst system selected from the group of $AlCl_3$/co-catalyst, H_3PO_4, and solid acidic resin catalysts.

32. The process of claim 21 further comprising the steps of:

(g) contacting at least a part of the light Fischer Tropsch liquid with a dehydration catalyst to dehydrate alcohols in the light Fischer Tropsch liquid to corresponding alpha- and internal-olefins to form a dehydrated product; and

(h) oligomerizing in the oligomerization reactor at least a portion of the dehydrated product produced in step (g) to form a product comprising a heavy branched olefin stream.

33. The process of claim 32 wherein the dehydration catalyst is selected from the group of treated activated alumina and treated activated silica-alumina.

34. The process of claim 32 wherein the dehydrated product of step (g) is fractionated to recover a C_9-C_{13} fraction and wherein the C_9-C_{13} fraction is the dehydrated light Fischer-Tropsch liquid used in step (d).

35. The process of claim 32 wherein the dehydrated product produced in step (g) is fractionated to recover a C_{14}-C_{18} fraction and wherein the C_{14}-C_{18} fraction is oligomerized in step (d).

36. The process of claim 32 further comprising the step of isomerizing at least a part of the dehydrated product of step (c) prior to oligomerization in step (d).

37. The process of claim 21 further comprising the steps of:

(i) fractionating the product of step (d) to isolate a nonoligomerized olefin/paraffin stream; and

(j) dehydrogenating the nonoligomerized olefin/paraffin stream by contacting it with a dehydration catalyst.

38. The process of claim 37 wherein the dehydrogenation catalyst is platinum supported on a high-surface alumina.

39. The process of claim 37 further comprising the step of:

(k) passing the product of step (j) into the oligomerization reactor.

40. The process of claim 21 further comprising the step of fractionating the synthetic lubricant crude basestock to recover a synthetic lubricant basestock product containing essentially no unsaturated hydrocarbons and essentially no hydrocarbons having a carbon number of less than 15.

41. The process of claim 1 wherein the synthesis gas is produced by autothermal reaction in the presence of nitrogen.

42. A high stability synthetic lubricant crude basestock produced by the process of claim 1 having a BI of between about 23.4% and about 25.5% and a DM of between about 18% and about 21.2% such that DM $\geq$ 2BI –29.9.

43. The high stability synthetic lubricant crude basestock produced by the process of claim 1 wherein the BI is between about 23.4% and 24.7% and the DM is between about 20.4% and about 21.2%.

44. The high stability synthetic lubricant crude basestock of claim 43 wherein the BI is about 24.4% and the DM is about 21.1%

45. A high stability synthetic lubricant crude basestock produced by the process of claim 1 having a BI of 25.5% or less and DM of 21.2% or lower such that DM $\geq$ 2BI –29.9.

46. A high stability synthetic lubricant crude basestock produced by the process of claim 21 having a BI of 25.5% or less and DM of 21.2% or lower such that DM $\geq$ 2BI –29.9.

47. A high stability synthetic lubricant crude basestock produced by the process of claim 21 having a BI of between about 23.4% and about 25.5% and a DM of between about 18% and about 21.2% such that DM $\geq$ 2BI –29.9.

48. The high stability synthetic lubricant crude basestock produced by the process of claim 21 wherein the BI is between about 23.4% and 24.7% and the DM is between about 20.4% and about 21.2%.

49. The high stability synthetic lubricant crude basestock of claim 48 wherein the BI is about 24.4% and the DM is about 21.1%

50. A lubricant baseoil composition produced by an integrated Fischer-Tropsch process comprising at least 40% of methyl branched hydrocarbons, characterized by BI of between about 23.4% and about 25.5% and a DM of between about 18% and about 25.5% and at least 5% long-chain branched hydrocarbons wherein the branches have a carbon number of at least 2, and are characterized by BI of less than about 24% and a DM of less than about 21%, wherein the lubricant baseoil arises from both Fischer-Tropsch oil and Fischer-Tropsch wax.

51. The lubricant baseoil composition of claim 50 wherein the methyl branched hydrocarbons are characterized by a BI of about 25% and a DM of about 20%.

52. The lubricant baseoil composition of claim 50 wherein the long-chain branched hydrocarbons are characterized by a BI of about 21% and a DM of about 19%.

53. A lubricant baseoil composition produced by an integrated Fischer-Tropsch process comprising at least about 40% of methyl branched hydrocarbons with a pour point of at most -10°C, and at least about 5% long chain branched hydrocarbons having a pour point equal to or less than -30°C.

54. A lubricant baseoil composition produced by an integrated Fischer-Tropsch process comprising at least about 40% of methyl branched hydrocarbons and at least about 5% long chain branched hydrocarbons wherein the baseoil composition has a pour point of about -20°C.

55. The process of claim 1 further comprising the step of fractionating the synthetic lubricant crude basestock.

56. A synthetic lubricant crude basestock produced by the process of claim 1 which comprises between about 15 and about 25 vol% 2cSt product, between about 15 and about 25 vol% 3 cSt product, between about 20 and about 30 vol% 5 cSt product, between about 20 and about 30 vol% 6 cSt product and between about 12 and about 18 vol% product having a viscosity of greater than 6 cSt.

57. A synthetic lubricant crude basestock produced by the process of claim 1 wherein 4 cSt and heavier products comprise at least 40% of the total lubricant crude basestock.

58. A synthetic lubricant crude basestock produced by the process of claim 21 which comprises between about 15 and about 25 vol% 2cSt product, between about 15 and about 25 vol% 3 cSt product, between about 20 and about 30 vol% 5 cSt product, between about 20 and about 30 vol% 6 cSt product and between about 12 and about 18 vol% product having a viscosity of greater than 6 cSt.

59. A synthetic lubricant crude basestock produced by the process of claim 21 wherein 4 cSt and heavier products comprise at least 40% of the total lubricant crude basestock.

60. The process of claim 1 wherein the lubricant crude basestock comprises 2 cSt, 3 cSt, 4 cSt, and higher cSt components and wherein the ratio of 2 cSt plus 3 cSt component to 4 cSt and higher cSt components is between about 0.8 and about 1.2.

61. The process of claim 18 wherein the Group VIII metal is palladium.

62. The process of claim 18 wherein the Group VIII metal is nickel.

63. The process of claim 18 wherein the high-surface inorganic support is high-surface alumina.

64. The process of claim 18 wherein the Group VIII metal is palladium and the high-surface inorganic support is high-surface alumina.